## Description of a case study

Anibal Bregon, Carlos Alonso-Gonzalez, and Belarmino Pulido

September 17, 2013

## 1 Case Study

A simple one tank system (Fig. 1).



Figure 1: Diagram of the tank system.

The system is represented by the following set of equations:

Constraint	Equation	Component	Fault
$c_1: (\dot{h}, Q_i, Q_o)$	$e_1: Ah = Q_i - Q_o$	Т	$f_T$
$c_2:(h,\dot{h})$	$e_2: h = \int_0^t \dot{h} \cdot dt$		
$c_3:(Q_o,u_c,h)$	$e_3: Q_o = K_c \sqrt{h \cdot u_c}$	$V_o$	$f_{V_o}$
$c_4:(u_c,h)$	$e_4: u_c = pid(h)$	PI	
$c_5:(h^*,h)$	$e_5: h = h^*$	LT	$f_{LT}$
$c_6:(Q_o^*,Q_o)$	$e_6: Q_o = Q_o^*$	$FT_1$	$f_{FT_1}$
$c_7:(Q_i^*,Q_i)$	$e_7: Q_i = Q_i^*$	$FT_2$	$f_{FT_2}$

Where  $Q_i$  and  $Q_o$  are the input and output flows to the tank, T, h represents the level of the tank, and  $u_c$  is the PID signal that controls the opening of valve  $V_o$ . A is the cross section of the tank, and  $K_c$  is the valve constant. Three sensors, LT,  $FT_2$ , and  $FT_1$  measure the variables h,  $Q_i$ , and  $Q_o$ , respectively, and we represent such values as  $h^*$ ,  $Q_i^*$ , and  $Q_o^*$ . In this plant, we consider faults in the level and output sensors,  $f_{LT}$  and  $f_{FT_1}$ , respectively, leakages in tank T,  $f_T$ , and partial blocks of valve  $V_o$ ,  $f_{V_o}$ .